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- (54) Electrostimulation of microbial reactions.
- (5) A method of fermanting a substrate with a microorganism by forming a broth comprising the substrate and the microorganism, and forming a fermantation product therefrom characterised in that a fermantation stimulating electrical signal is imposed seroes the broth.

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DESCRIPTION

"ELECTROSTIMULATION OF MICROBIAL REACTIONS"

Microbe reactions, i.e., fermentation, are the biological conversion of a feedstock, i.e., a substrate, to a metabolite, i.e., a product, by the actions of 5 microbes. Microbe reactions are characterized by the growth of the microbe, and the subsequent formation of a metabolite product. That is, substrate is used initially for the growth and maintenance of the microbes. and subsequently for both the growth and maintenance of the microbes and for the formation of product. formation is related to the concentration of substrate; ' the concentration of microbes, and the yield coefficients of product and microbes with respect to the substrate. Moreover, the concentration of microbes is a function of the specific growth rate of the microbes, and the yield 15 coefficient of the microbes with respect to the substrate.

That is, they require long residence time, i.e, high ratios of reaction medium volume per unit volume of production per unit time. They also have a long initiation time. That is, metabolite product cannot be formed in large quantities until high concentrations of microbe are present. Nutrient, i.e., substrate, is initially utilized primarily to grow and maintain microbes, and there-after it is utilized to a greater extent to form metabolite product.

Moreover, the reactions, involving microbial growth and division, are complex. For example, when the microbes are bacteria, cell growth and division is by 30 fission, i.e., an individual cell will double in mass and content of cell constituents, and then split into two identical daughter cells. By way of contrast, yeasts are a class of microorganism that grow and divide by budding. That is, a bud will grow on an individual cell

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until it matches the size of the original cell, and then separate, leaving a bud scar. Fungi grow by chain enlongation and branching, i.e., with growth proceeding from the tip of the mycelium through the formation of septa between individual cells. Cell division may require anywhere from 15 minutes to an hour for bacterial growth, from 45 minutes to 2 hours for yeast growth, and from one to eight hours for fungi or mycelial growth.

The specific path of product synthesis, i.e., the reaction path for the formation of the metabolite product from the substrate or nutrient is not clearly understood for every fermentation reaction. However, it is believed to depend upon microbe growth and concentration, nutrient utilization, and metabolic controls.

It has now been found that the reaction rate of fermentation reactions, that is, the yield per unit time, unit volume, unit nutrient or substrate concentration, and unit microbe concentration is enhanced by the application of an alternating or pulsed high frequency electric field to the reaction medium of microbes, substrate, and nutrients.

As used herein, the terms "fermentation",
"formentation reactions", and "reactions utilizing
fermentation techniques" include aerobic and anaerobic
metabolic activity of a microbe or microbes in which
chemical changes are brought about in an organic or
inorganic substrate, and any process mediated by or
involving microbes or microorganisms in which a product
accrues.

As used herein, the terms "microbes", "microbe", microorganisms", and "micro-organisms" include prokaryotes and eukaryotes. "Trokaryotes", as used herein, means unicellular microorganisms, including bacteria and unicellular blue-green algae. "Eukaryotes", as used

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herein, means multi-cellular microorganisms, including fungi, yeasts and actinomyoetcs. As used herein, the terms "microbes", "microbes", "microorganisms" and "micro-organisms" include immobilized microbes and systems and structures of immobilized microbes as well as non-immobilized microbes. As used herein, the terms "microhes", "microbe", "microorganisms", and "microorganism" include both naturally occurring strains and artificial recombinant strains.

Fermentation reactions, i.e., fungus, yeast, actinomycotes, and bacterial fermentation reactions are
utilized industrially. Fermentation reactions are capable
of wider industrial use based upon raw material availability and costs, by-product usage, and increased
reaction rates.

According to the invention described herein, any or all of the reaction rate, the innoculum build up, or efficiency of conversion are increased by electrical stimulation. Electrical stimulation may be utilized to 20 reduce the time required to carry out the reaction or to increase the productivity of a given unit of production, that is to increase the number of batches that can be fermented in a given reaction vessel.

By electrical stimulation is meant the application

25. of a pulsed or alternating high frequency electric
signal field across the broth whereby to pass an electrical
current through the broth, e.g., by inserting electrodes
in the broth, under conditions which increase the rate
of the microbial reaction, while substantially avoiding

30 significant destruction of the micro-organisms, e.g.,
fungi, bacteria, yeasts or actinomycetes, the reactants,
e.g., the substrate, or the products.

It has been found that a frequency of from about 1 kilohertz to about 1000 kilohertz is particularly satisfactory in carrying out the method of this invention.

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The electrical stimulation electrical current may be an alternating current or pulsed direct current. It should have a frequency of from about 1 kilohertz to about 1000 kilohertz, although frequencies below about 10 megahertz may be used as well as frequencies above about 0.1 kilohertz with some increases in yield. However, care should be taken e.g. by using a frequency above about 0.1 kilohertz, to avoid large amounts of electrolysis occurring within the reaction medium at low frequencies.

The method of this invention may advantageously be carried out at various ranges of the electrolytic variables, i.e., electrode area, inter-electrode spacing, inter-electrode volume, current, current density, current per unit inter-electrode volume, current per unit broth volume, voltage, voltage per unit inter-electrode volume, power per unit inter-electrode volume, power per unit broth volume, and frequency.

For example, the method of this invention has been carried out utilizing Saccharomynes cervisiae to ferment glucose at currents per unit interelectrode volume of from about 1 x 10-3 milliamperes per cubic centimeter to about 30 x 10⁻³ milliamperes per cubic centimeter of inter-electrode volume, at currents per unit broth volume of from about 1 x 10-4 milliamperes per cubic centimeter to about 50 x 10-4 milliamperes per cubic centimeter of broth, current densities of about 2 x 10-2 milliamperes per square centimeter to 5 x 10-1 milliamperes per square centimeter of electrode area, voltage fluxes of Q.1 to 3 millivolts per centimeter of inter-30 electrode space, interelectrode power dissipations of 0.2 x 10⁻⁷ watts per cubic continctor to 6 x 10⁻⁷ watts per cubic centimeter of interelectrode volume and brothpower dissipations of 0.2 x 10⁻⁸ watts per cubic centimeter of broth volume to 8 x 10⁻⁸ watts per cubic

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centimeter of broth volume. Electrolytic variables, i.e. currents, voltages, and power dissipations, and products and quotients thereof, outside the above ranges may be utilized as long as care is taken, by avoiding simultaneous astomer of the ranges, to avoid destruction of the microbes.

According to one exemplification of the method
herein contemplated, a reaction medium of a hexose,
e.g., glucose, other nutrients, and a yeast, Saccharomyces
cerevisiae is provided. A pair of electrodes are spaced
about 4 to about 7 centimeters from each other within
the broth, and an electrical current at a current density
of about 0.1 to about 0.3 milliemperes per square
centimeter of electrode area is passed through the
reaction medium at a frequency of about 100 kilohertz to
about 1000 kilohertz. In this way, the yield of product
per unit of substrate per unit time is increased by
about 15 to about 20 percent compound with the result
without electrical stimulation.

According to an alternative exemplification of the method of this invention, a reaction broth of a bacterium such as Bacillus polymyta or Bacillus licheniformis, and glucose are prepared. The fermentation reaction is then carried out while an alternating current having a frequency of about 1 kilohertz to about 1000 kilohertz, an imposed voltage signal sufficient to provide a current of 1 x 10⁻³ milliamperes per cubic centimeters of interelectrode volume and 10⁻¹ to 5 milliampers per liter of colution is imposed across the broth. The resulting production rate of butane diol is increased by about 20 percent compared with the result without electrical stimulation.

The method of electrostimulated fermentation herein described is useful with single cell blue-green algae, 35 bacteria, yeasts, and actinomycetes. Suitable yeasts are for example, beker's yeast and brewer's yeast, i.c.,

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single cell yeart of the Saccharomycoidicae group, as exemplified by Saccharomyces cerevisiae.

The method of cleetrostimulated fermentation is useful with various feedstocks. Exemplary are various carbohydrate substrates. By carbohydrates we meen for 5 example polyhydroxy alkehydes, polyhydroxy ketones, and substances that yield polyhydroxy aldchydcs or polyhydroxy kelones upon hydrolysis or saccharification. Exemplary carbohydrates are sugars, i.c. caocharides. The saccharides useful in the method of this invention 10 may be monosaccharides, i.e., carbohydrates incapable of further hydrolysis, or polysaccharides, i.e. carbohydrates that yield monosaccharides upon hydrolysis or sacchar-Naturally occurring saccharides useful as substrates in the methods of this invention include 15 heptoses, hexoses, pentoses, tetroses, triose, homopolysaccharides thereof, and heteropolysaccharides thereof. Exemplary hexoses include glucose, fructose, mannose, galactose, and the fructose-glucose dissacharide, sucrose. Exemplary pentoces include arabinose, wylose, ribose, and 20 apiose. Exemplary polysaccharides include sucrose, mentioned above, maltose, lactose, raffinose, starch, glycogen, cellulose, pectins, chitin, inulin, agar, hemicelluloses, plant gums and mucilages, and immunopolysaccharides. By carbohydrales we also mean sugar 25 alcohols, e.g. sorbitol, mannitol, glactitol, or the inositols. Industrial sources of carbohydrate include by way of exemplification manure, cellulosic wastes, molasses, whey, sugar, grain starches, and byproduct carbohydrates. Suitable grain starches include by way **30**. of exemplification corn, corn stoyer, wheat, barley, straw, and bagasse.

Amino acids may be utilized as substrates for fermentation type reactions. They may be recovered as products of fermentation type reactions, or they may be

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intermediates, produced in one fermentation type reaction as a substrate for a subsequent fermentation type reaction. Exemplary alpha-amino acids include glycine, alanine, valine, leucine, isoleucine, serine, threonine, cysteine, cystine, methionine, phenylalenine, tyrosine, proline, tryptophan, lysine, arginine, histidine, aspartic acid, and glutamic acid. The above cnumeration is intended to be exemplary and not exclusionary.

Other substrates which may be utilized are, for example, hydrocarbons, e.g., aliphatic hydrocarbons, 10 earbocyclic hydrocarbons, and heterocyclic hydrocarbons. As used herein, hydrocarbons include substituted hydrocarbons, e.g. halogenated hydrocarbons, and hydrocarbons . having one or more functional groups, e.g. alcohol, ketono, aldehyde, acid, ether, smine, amidine, N-alkyl amide, N.N-dialkyl amide, imidic ester, imide, aldimine, ketimine, thiol, thio ether, disulfide, thio acid, dithioacid, thio aldehyde, thio ketore, sulfonium, sulfoxide, sulfinic acid, sulfone, sulfonic acid, phosphite, phosphine, phosphonate, phosphate, orthocarbonate, 20 carbonate, chloroformate, carbamate, carbamide (including urca), M-alkylurca, o-alkylurca, cyanate, isocyanate, carbodiimide, xanthate, thiocarbamate, thiocyanate, inothiocyanate, diazoate, or diazocyamide groups. 25 many cases the substrate is a dilute pollutant, and is degraded or metabolized to a non-polluting product.

The method of electrostimulated fermentation may be utilized with both aerobic and anaerobic fermentations.

Electrostimulated fermentation is useful in the industrial scale production of any product that can be produced by fermentation techniques, as described hereinabove. These products include the following, which enumeration is exemplary and not exclusionary: enti-hiotics; organic solvents, for example alcohols, e.g., butanol, ethanol, and amyl alcohols, ketones e.g. acetone;

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gases, e.g. carbon dioxide and hydrogen; beverages, e.g. wines, heers and liquors; foods, e.g. cheeses, fermented milks, pickles, sauerkraut, soy sauce, yeast, vinegar, and mushrooms; flavoring agents e.g. monosodium glutamate; organic acids and hydroxy acids e.g. lactic acid, acetic seid, citric scid, gluconic scid, butyric scid, fumaric acid, and itaconic acid; glycerol; amino acids, e.g. L-glutamic acid and L-lysine; steroids; organic transformations, including steroid, alkaloid, and antibiotic transformations; yeasts, including food yeasts and 10 animal feed yeasts, legume innoculants; pesticides, c.g. microbial and racterial pesticides; vitamins and growth stimulants, e.g. vitamin B 12 vitamin A, riboflavin and gibberalkines; enzymes including amylases, proteolytic enzymes, pectinases, invernases, and cellulases, inter alia; fats; fatty acids; alcohols; fuels; and hydrocarbons.

The electrostimulation method herein contemplated may also be used for the control or destruction of leleterious substances, e.g., pollutants, and aqueous dispersions, suspensions and solutions of hydrocarbons or halocarbons, including polymers thereof.

While the electrostimulate fermentation method described herein above is useful with various microbes in various fermentation reactions, the method of this invention may be exemplified by the Weizmann Process for the bacterial fermentation of starch to yield n-butyl alcohol, ethyl alcohol, and acetone; the production of ethyl alcohol by the use of <u>Phizopus formosaensis</u>, <u>Saccharomyces cervisae</u>, <u>Saccharomyces uvarium</u>, or <u>Aspergillus foetidus</u>; the production of acetic acid utilizing <u>Acetobactel alcoholophilus</u>, <u>Lactobacillus</u> plantarum, or <u>Polyporus palustris</u>; the production of acetone utilizing <u>Clostridiums</u>; the production of butanol utilizing <u>Clostridiums</u>; the production of glycerol

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utilizing Bacillus licheniformus or Saccharomyces rouxii; the production of acetic acid using Acetobactei pasteurianus; the production of wines using Saccharomyces chevalieri, Saccharomyces ocrvisiae, Saccharomyces roei, Saccharomyces vafer, Saccharomyces vini, Torulaspora 5 florentina, Saccharomycca aceti, or Saccharomyces oxidans; the production of edible proteins utilizing C. hactomium cellalolytilum, Geotrioum candidum, Caudida utilis, Collulmonas or Alcaligenes faecalis; the production of anthroquinones utilizing Chrysosporium merdarium, 10 Helminthsporium cynadonitis, or Penicillium islandicum; the production of antibiotics utilizing Byssochlamys nivea, Fusarium equiseto, Gliocladium, Aspergillus aptienus, Aspergillus sulphureus, Penicillium cyclopium, Penicillium martensi, Penicillium palitans, Penicillium puberalum, 15 Aspergillus nidulans, Penicillium ohryogenum, Penicillium notatum, acromonium strictum, Cephalasporium chrysogenum, Serratia rebidaea, Streptomyces lavendulae, Streptomyces clauligous, Streptomyces lipmanii, Acinetobacter calcoaceticus, Bacillus ceres, Hacillus licheniformis, or 20 Bacillus subtilis; the production of L-arginine by Bacillus subtilis, Breribacterfum flurum, Corynebacterium glatamicum, or Protamino bacter thiaminophagus; the production of ascurbic acid by escherichia; the production of biotin by Corynebacterium primorioxydans, or Psuedo-25 manus mutablic; the production of butanediols using Racillus licheniformis, Escillus polymyxa, or Klebsiella pneumoniae; the production of butyric acid using hutyrivibrio fibrisulvens; the production of caprylic acid using Ramibacterium alactolyticum; the production of carboxylic acid utilizing Succhromycopsis linelytica, or Sporolomyces odorus; the production of formic acid using Polyporus palustris; the production of fructose utilizing Bacillus megaterium, Pseudomanus borcopollis or Pseudomonas fluorescens; the production of gluconic acid using 35

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Aspergillus carbonarius, or Penicillum chrysogenum; the production of glucose utilizing Trichoderma longibrachiatum; the production of p-hydroxy benzalathyde using Gaccharomyces satic; the production of single cell proteins utilizing Arthrobacter petrolcophagus, Arthrobacter rubellus, Arthrobacter, Aspergillus fumigatus, Cellulomonas cartelyticum, Corynebacterium fujiokemse, Kluyuromyces fragilis morehella crassipe, Mycobacterium cureatum, Mycocbacterium vetrolcophilum, or Nocardic necopaca, and the production of xenthar gum using, e.g., Xanthamonas campestris. The method of electrostimulated fermentation may be used in the fermentation of substrates to obtain vitamins, antibiotics, and enzymes.

Electrostimulated fermentation also finds utility 1.5 in microbial cellulose digestion, e.g., with Polyangium cellulosum; cleaning metallic surfaces, e.g., with Thiobacillus ferrooxidans or Thiobacillus thiooxidans; degradation of cellulose; degradation of cyanides in waste water, e.g., with Bacillus subtilis, Corynebacterium, 20 or Nocardia rubropertincta; degradation of ethylene glycol with unidentified bacterium, ATCC 27042; degradation of chlorinated phenol fungicides; degradation of systemic fungicides, e.g., with Rhizopus japonicus; degradation 25 of hydrocarbons, c.g., with Aspergillus versicolor, Brettznomyces petrophilum, Candida petrophilum, Candida tropicalis, Claclosporium resinae, Cunninghamella elegans, Eupenicillium zonatum, Saccharomycanoris lipulytica, or Morulopsis petrophilum; degradation of jet fuel, 30 e.g., with Acremonium strietum, Alternaria alternata, Aspergillus jumigatas, or Cladosporium resinae; degradation of methanol, e.g., with Hausenula polymorpha; degradation or nitriles in waste water, e.g., with Alcaligenes visolactis, Nocardia rubroutineta, or

35 Bacillus subtilis; degradation of petroleum, e.g. with Aspergillus aurochasidium, Candida parapsilusis, Candida

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Myrothecium verrucaria, Mocardia corallina, Nocardia Eloberula, Nocardia opain, Nocardia paraffinae, Mocardia rubra, Penicillium, Prototheca, Rhodotorula, Saccharomyces carvisiae, or Saccharomycesis lipolytica; the degradation of phenol, e.g., with Glosoporus dichrous, or Rhodutorula glutinis; the degradation of wood; phosphate removal in sewage treatment, e.g., with Chrysosporium pannorum, Geotrichum candidum, Mucar hiemalis, and Faecilomyces carneus; water pollution control, e.g., with Rhodotorula glutinis and Trichothecium roseum; and the production of dextrans by the fermentation of sucrose, e.g., with Leuconostoc mesenteroides and Betacoccus arabino sareus; and the production of immunopolysaccharides.

The following examples are illustrative:

EXAMPLE I

Electrostimulated and conventional fermentations were carried out in a batch reactor.

The reaction broth was propared by placing 1500 milliliters of distilled water in a sterilized 3 liter beaker. Carbohydrates, water and nutrients were added to the beaker in the following quantities:

			Glucose			220 grams
25	٠	٠.	NaCl	•	• • •	3. grans
•••			(NH ₄) ₂ 50 ₄			6 grams
• •	-		K ² HPO ⁴	•	•	2.4 grams
			KH ⁵ FO ⁴		•	0.4 grams

Distilled Water to make 2 litero

Thereafter, a 200 milliliter portion of the glucose solution was placed in a sterilized container and 14 grams of Fleischmann's Baker's Yeast, Succharomyces ocrevisae, was added thereto and stirred to form a slurry. The yeast-glucose slurry was divided into two equal

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portions of 100 milliliters each and put into two'l liter sterilized resin kettles. To each of the divided yeastglucose slurries were added 2.1 grams of corn meal, and
700 milliliters of the glucose solution.

The outlets of both reactors were connected to wet test meters to measure the gas produced. One reactor was run without electrical stimulation.

The other reactor had an electrode pair of two 4 square inch stainless steel electrodes, 4 centimeters apart. A signal generator was utilized to generate a 300 kilohertz, sine wave, voltage signal. A 50 milivolt signal caused a current of 1.5 milliamperes to flow.

Eight simultaneous, side-by-side runs were made, with one reactor having electrical stimulation and the other reactor being unstimulated.

The results shown in Table I, below, were obtained;

TABLE I

COMPARISON OF ELECTRO-STIMULATED FERMENTATION WITH

CONVENTIONAL FERMENTATION

	Iength of Mun (hours)	Current (milli- amperes)	Moles of Ethanol- Stimulated (gel chro- matographic)	Moles of Ethanol- Unstimulated (gel chro- matographic)
25	26.5	1.25	0.476	0.456 .
	19	1.25	0.506	0.475
	22	. 1.5 .	0.561	0.469
•	47-5	1.5	0.967	0.930
	23.4	2.25	0.840	0.855
30	27	2.5	0.420	0.390
	43.4	1.5 -6.1	1.14	1.16
	25.5	2.25-6.5	0.713	0.707
		•		

EXAMPLE II.

Electrostimulated fermentation was carried out in 35 a batch reactor to determine the effect of current and frequency.

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The reaction broth was prepared by placing one liter of distilled water in a sterilized beaker. Carbohydratos, water and nutrients were added to the beaker in the following quantities:

Sucrose 100 grams/liter

NaOl 1.5 grams/liter

(NH₄)₂SO₄ 3.1 grams/liter

K₂HPO₄ 1.2 grams/liter

KH₂FO₄ 0.2 grams/liter

Distilled water

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1.2 liters of the solution were placed in a 1.5 liter resin kettle.

Thereafter, 7.0 grams of Fleischmann's dried Baker's Yeast, saccharomyces occevisiae, was poured on top of the reaction broth. The reactor was then closed, with gas venting through a water scal bubbler. The mixture was allowed to stand for 18 hours.

Thereafter, at 24 hour intervals, the slurry was removed from the reactor by aspiration and filtered to recover the yeast cake. The yeast cake was added to 1.0 liter of fresh reaction broth and returned to the kettle, which was sealed with a gas vent to a burette of 1 percent sulfuric acid and stirred for 5 minutes.

After two hours, four gas volume readings were taken at one half hour intervals, and used to calculate a base gas evolution rate, Ro. Thereafter, electrical stimulation was commenced. Four gas volume readings were taken at half hour intervals beginning one hour after electrical stimulation, and used to calculate a test gas evolution rate, R_T. For the fermentation with electrostimulation, R_T is the gas evolution rate. For the fermentation without electrostimulation, R_T is the gas evolution rate gas evolution rate measured simultaneously with and calculated in the same way as the gas evolution rate for electrostimulation. After three hours of electrical stimulation,

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the current was turned off for 19 hours, and then reaction slurry removed as described above.

hach electrode was a nickel wire, 0.63 millimeters diameter, spiraled twice around a four inch (10 cm) long, 5 millimeter diameter glass rod. The electrodes were spaced 6.5 to 7.0 centimeters apart. Vultage was provided by a Dynascan 3010 function generator.

The effect of applied electrical field was as shown in Table II below:

TABLE II

EFFECT OF APPLIED CURRENT (AT 100 KILOHERTZ)

ON GAS EVOLUTION

15	Current (milli- amperes)	(R _m /Ro) (without current)	(R _m /Ro) (with current)	(R _p /Ro) with current (R _p /Ro) without current
	. 0.15	·1 - 05	1.15	1.10
	0.15	0.92	1.02	1.11
	1.5	. 1.01	1.13	1.32
20	1.5	0.98	1.17	1.19

The effect of frequency was as shown in Table III below:

EFFECT OF FREQUENCY (AT 0.15 MILLIAMPERES)
ON GAS EVOLUTION

٠.	Frequency (kilohertz)	(R _T /Ro) - (without current)	(R _T /Ro) (with current)	(R _T /Ro) with current (K _T /Ro) without current
30	10	0.83	0.92	1.11
	100	1.05	1.15	1.10 ·
	100	0.92	i.02	1.11

EXAMPLE TIT

Fermentation of glucose with <u>s.cervisiae</u> was carried out with and without electrical stimulation.

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A broth was prepared containing 220 grams of glucosc, 7.5 grams of S.cerevisae, 10 grams of NH₄Cl, 22 grams of Na₂HPO₂ x 7 H₂O, 12 grams of KH₂PO₄, 1 gram of MgSO₄, and 0.04 grams of CaCl₂, and distilled water to make two liters.

The broth was divided into two portions and placed in sterilized resin kettles. Both kettles were stirred continuously with a magnetic stirrer. One kettle, intended for electrostimulation, had an electrode pair, each electrode was a 0.63 millimeter diameter nickel wire spiraled twice around a four inch (10 cm)long, 3 millimeter diameter, glass rod. The electrodes were spaced 6.5 to 7.0 millimeters apart.

The fermentation was carried out at 30 degrees Centigrade for 23.5 hours. A signal generator was utilized to generate a 300 kilohertz, 50 millivolt, sine wave signal. The results shown below were obtained:

S. CERVISIAE FERMENTATION OF GLUCOSE

_			 .
20 · .		WITHOUT ELECTRICAL STIMULATION	
	FREQUENCY	******	300 kilohertz
•	CURRENT	· · ·	1.5 milliamperes
25	INITIAL YEAST (GRAME/		r.> writismberes
•	LITER)	5. 4	5-5
	FINAL YEAST (GRAMS/		•
٠.	LITER)	8.8	9.3
30	INITIAL GLUCOSE (GRAMS/ LITER)	. 108.9	106.3
	FINAT, GLUCOSE (GRAMS/ .		
	· LITER)	4.3 .	<0. 20
•	TNITIAL ALCOHOL (GRAMS/LIT	ER) 0.7	. 0.8
	FINAL ALCOHOL (GRAMS/LITER	43.0	54.4
35	GRAMS OF YEAST/GRAMS OF		
		.18 x 10 ⁻³	2.83 × 10 ⁻³
•	GRAMS OF ALCOHOL/GRAMS OF GLUCOSE-HOUR	-71 × 10 ⁻²	2.18 x 10 ⁻²
h. a	GRAMS OF ALCOHOL/GRAMS		2020 2 20
40	OF YEAS'! (FINAL)	4.87	5.72
		•	• •

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CEIT. COUNT OF 200 SQUARES (three pipette samples per kettle)

•	. Sample 1	660 ·	865
	SAMPLE 2	7 39	895
5	. Sample 3	632 .	804
	MGAN	. 677	855
	rance	107	91
	STANDARD DEVIATION	63	53
10	PERCENT RETATIVE STANDARD DEVIATION	9.3	6.2
	DIFFERENCE IN MEANS	178	
	·	6	

$$\sqrt{\frac{\sigma_1^2 + \sigma_1^2}{n_1}} = \frac{\sigma_1^2}{n_2}$$

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26 + 7% RELATIVE (at 1 standard deviation level)

(61 is the stranded deviation and n₁ is the number of replications).

The student's "t" test was applied to the cell counts. A Qt of 3.79 with a probability of 0.02 was obtained. That ic, the probability that random errors would result in the 26% relative difference observed was less than 2 percent.

EXAMPLE IV

A series of tests were conducted to compare electrostimulated fermentation with conventional 25 Termentation. For each test a simple nutrient solution was prepared. A portion of the nutrient solution was withdrawn to make a yeast solution. The remainder of the nutrient solution was divided into two equal portions and placed into two identical laboratory 30 Both fermenters had an electrode pair. fermenters. Fleischmann's Baker's Yeast, Saccharomyces cervisiae, was slurried in the remainder of the single nutrient solution. The nutrient solution, containing the yeast, was divided in half. Each half was placed into one of 35 the two identical laboratory fermenters. A voltage

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signal was applied across one solution only of the pair. Solution samples were simultaneously taken from both solutions of the pair. Differences between the two fermentations of a pair were attributed to electroctimulation, while differences between sets of pairs of fermentations were attributed to conditions of the nutrient and innoculum solutions prior to commencing the tests.

For each fermentation a resin kettle fermenter was used. The resin kettle fermenter had an inside diameter of 10 centimeters, a depth of 15 centimeters, and was sealed on top. Each recin kettle fermenter had a sample probe, a pH probe, a mechanical stirrer, a sodium hydroxide inlet, a gas outlet, and an electrode pair. The electrodes were a pair of two inch (5 cm) by two inch (5 cm) stainless steel plate electrodes opaced two inches (5 cm) apart.

A glucese solution was prepared by adding in order: Glucose • H₂O 220 grams.

The glucose solution was builted, and the pH was adjusted to pH--5 with $H_{\rm z} H O_{\rm h}$.

A yeast slurry was prepared by withdrawing 200 milliliters of the glucose solution, and stirring 3.6 grams of Fleischmann's Baker's Yeast Eacharomyces cervisiae into the nutrient.

Fach test was commenced by dividing the nutrient solution into two 800 milliliter portions and placing

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one portion of the nutrient solution into each resin kettle fermenter. Thereafter the slurry of yeast and nutrient was divided into two 100 milliliter portions. One portion of the yeast-nutrient slurry was added to each of the resin kettles.

The resin kettles were maintained at a temperature of 30 degrees Centigrade by immercion in a water bath. The pH was maintained between pH 4.7 and pH 5.2 by addition of aqueous NaOH. In each run a 300 kilohertz, 1.5 milliampere, 50 millivult signal was applied across the electrone pair in one kettle. No signal was applied to the electrode pair in the other kettle.

The following results were obtained:

	Sct 1				•
15	ELAPSED	<u>ио с</u>	URRENT	CUR	RENT
	TIME	Ethyl		Ethyl	
		Alcohol	Glucose	Alcohol	Glucose
20	(hours)	(grms/ liter)	(grms/ litcr)	(grms/ liter)	(grms/ liter)
	1.25	1.17	98	.72	. 100
-	. 3	1.87	96	1.96	98 .
	6	. 5.28	78	5.72	79
	25	31.8	6.25	40.4	(0. 25
25	Final Yeas (grms/lite		54`.	2.6	3
	Bet 2		.	•	
				,	
:	ELAPSED	NO C	URRENT	- <u>Cur</u>	RENT
: 30		Ethyl .			RENT ·
: 30	ELAPSED	Ethyl Alcohol	Glucose	Ethyl Alcohol	Glucose
30	ELAPSED	Ethyl .		Ethyl	Glucose
30	etapsed Time	Ethyl Alcohol (grms/	Glucose	Ethyl Alcohol (gims/	Glucose (grws/ liter)
30 35	ETAPSED TIME (hours)	Ethyl Alcohol (grms/ liter)	Glucose (grms/ liter)	Ethyl Alcohol (grms/ liter)	Glucose
	ETAPSED TIME (hours)	Ethyl Alcohol (grms/ liter)	Glucose (grms/ liter) 98 85	Ethyl Alcohol (grms/ Liter)	Glucose (grws/ liter) 103 98
	ELAPSED TIME (hours) 1 2	Ethyl Alcohol (grms/liter) 0.09	Glucose (grms/ liter) 98	Ethyl Alcohol (grms/ liter) 0.09	Glucose (grws/ liter)
	ELAPSED TIME (hours) 1 2 4.5	Ethyl Alcohol (grms/liter) 0.09 0.53	Glucose (grms/ liter) 98 85 78	Ethyl Alcohol (grms/ liter) 0.09 0.71 2.2	Glucose (grws/ liter) 103 98 76 64
	(hours) 1 2 4.5 6.5	Ethyl Alcohol (grms/liter) 0.09 0.53 2.7 5.6 40.2	Glucose (grms/ liter) 98 85 78 72 (0.25	Ethyl Alcohol (grms/ liter) 0.09 0.71 2.2 6.9	Glucose (grms/ liter) 103 98 76 64 (0.25

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Set 3			•	
ELAPSED TIME	. NO C	URRENT	<u>curi</u>	ENT
	Ethyl Alcohol (grms/	Glucose (grms/	Ethyl Alcohol (grms/	(fincose
(hours)	<u>liter)</u>	liter)	liter)	liter)
1	3.0	· 87	3.5	88
3	8.5	87	11.0	70
4.5	22.9	40	28.0	45
6	37.9	19	37-0	19
22.5	44.2	(0.25	48.7	(0.25
Final Yeast (grms/liter)	9.0		9.8	
Set 4		•		•
ELAPSED TIME	NO C	UBRENT	CUR	RENT
(hours)	Ethyl Alcohol (grms/ liter)	Glucose (gims/ liter)	Ethyl Alcohol (grms/ liter)	Glucose (grms/ liter)
ı	0.7	105	0.6	110
2	2.9	98	2.5	· 95
3	3.1	84	. 3.4	92
4 '	5.2	78	5.4	.82
· ·	11.6	60	10.5	62
G	18.7	10.2	19.9	1:0.3

27.1

32.0

51.0

56.0

-3

⟨0.25

Final Teast (grms/liter) 8.9 9.6

(0.25

24.8

31.9

41.7

46.0

8

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	Bet 5				
	ELAPSED TIME	<u>MO</u>	CURRENT	CUR	RERT
5	(hairs)	Ethyl Alcohol (grms/ liter)	Glucose (grms/ liter)	Ethyl Alcohol (grms/ liter)	Glucose (grms/ liter)
	ı	1.0	109	. 1.1	107
.•	2	2.0	90	2.8	97
10	ż	4.9	81.	5.1	83
	4	9.5	80	8.0	80
	5 ·	17.0	70	17.3	69 .
	6	19.1	54	17.7	56
	7	21.7	35 ·	24.0	39 ·
15	8	32.4	21	37.1	27
	23.5	41.4	. 4	46.9	(0.25
. •	Final Yea (grms/lit	st (er) 9	· •9	10.	5

while the invention has been described with respect to certain exemplifications and embodiments, that is with respect to certain microbes, i.e., bacteria, actinomycetes, fungi, and yeasts, certain substrates, i.e., hydrocarbons, and carbohydrates, and certain products, it is not to be so limited, except as in the claims appended hereto.

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-21-CTAINS

- 1. A method of fermenting a substrate with a microorganism by forming a broth comprising the substrate and the microorganism, and forming a fermentation product therefrom characterised in that a fermentation stimulating electrical signal is imposed across the broth.
- 2. A method according to claim 1 characterised in that the microorganism is yeast, actinomycetes, bacteria, or unicellular blue-green algae.
- 3. A method according to claim 2 characterised in that the yeast is a <u>Saccharomyoideae</u> or a <u>Sacchar</u>
 - 4. A method according to claim 1, 2 or 3 characterised in that the substrate is a carbohydrate, hydrocarbon or amino acid.
 - 5. A method according to olaim 4 characterised in that the carbohydrate is glucose, fructose or mannose.
- 6. A method according to claim 4 characterised in that the carbohydrate is a polyeacoharide.
 - 7. A method according to any of claims 1 to 6 characterised in that the electrical signal is an alternating current signal or a pulsed direct current signal.
- 25 8. A method according to any of claims 1 to 7 characterised in that the electrical signal has a frequency of 0.1 kiloherts to 10 megaherts.
 - 9. A method according to any of claims 1 to 7 wherein the electrical signal has a frequency of 1 kilohertz to 1000 kilohertz.
 - 10. A method according to any of claims 1 to 9 characterised in that the current per unit of interelectrode volume is from 1 x 10^{-3} to 30 x 10^{3} milliumperes per cubic centimeter.
- 55 11. A method according to any of claims 1 to 10 characterised in that the current per unit of broth is

from 1 x 10^{-4} to 50 x 10^{-4} milliamperes per cubic contineter.

- 12. A method according to env of claims 1 to 11 characterised in that the current density is from 2 x 10^{-2} to 50 x 10^{-2} milliamperes per square centimeters.
- 15. A method according to any of claims 1 to 12 characterized in that the voltage flux is 0.1 to 5 millivolts per centimeter.
- 14. A method according to any of claims 1 to 15 to characterised in that the interelectrode power dissipation is from 0.2×10^{-7} to 6×10^{-7} watts per cubic centimeter of interelectrode volume.
 - 15. A method according to any of claims 1 to 14 characterised in that the broth power dissipation is from 0.2 x 10⁻⁸ to 8 x 10⁻⁸ watts per cubic centimeter of broth.

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EUROPEAN SEARCH REPORT

EP 01 Application Application

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